

The chemical reaction kinetics study for the absorption of carbon dioxide into the aqueous diethylethanolamine/diethylenetriamine solutions

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1. Introduction –Alkanolamines and their blends are most widely used in the natural gas industry, oil refineries, petroleum chemical plants, and synthetic ammonia plants for the removal of acidic components, such as CO₂ and H₂S, from gas streams[1]. Different solvent systems are still undergoing development as the search for better performance in high CO₂ loading, the fast absorption rate and the less environmental impact [24]. The diethylethanolamine (DEEA) has been shown to have a higher carbon dioxide solubility and a lower absorption heat than those of monoethanolamine (MEA) and N-methyldiethanolamine MDEA[5]. Also polyamines have more than one amine functionalities which allow high absorption capacity and fast reaction kinetics compared to solvents with a single amine group [2, 6]. In this study, blended amines containing the tertiary alkanolamines DEEA and a polyamine DETA are considered as a potential CO₂ absorbent. Thus, the reaction kinetics of absorption of CO₂ into the aqueous diethylethanolamine (DEEA) + diethylenetriamine (DETA) solutions was studied using a wetted wall column apparatus. The density, viscosity, Henry's constant and diffusivity coefficient of CO₂ in the aqueous amine solutions at different temperatures were also measured. The reaction rate constants were determined from the measured specific absorption rate data. The results of the present study are in general with the accuracy in the carbon dioxide absorption process design calculations using aqueous DEEA + DETA solutions as the CO₂ absorbents. 2. Experimental - A short wetted-wall column was used to measure the CO₂ absorption rate. Figure 1 shows the wetted-wall column for measuring the CO₂ absorption specific rate. 3. Results and Discussion - The reaction rate constants were determined from the measured specific absorption rate data using the pseudo-first order reaction mechanism for the reaction of CO₂ with DEEA and the zwitterion mechanism for CO₂ with DETA. 4. Conclusions - The results of this study can be used for CO₂ absorption process design calculations using aqueous DEEA + DETA solutions as the CO₂ absorbent. 5. References [1] A. L. Kohl, and R. B. Nielsen, Gas purification, 5th ed., Houston, USA: Gulf Publishing Co., 1997. [2] S. Ma'mun, H. F. Svendsen, K. A. Hoff, and O. Juliussen, "Selection of new absorbents for carbon dioxide capture," Energy Convers. Manage, vol. 48, no. 1, pp. 251–258, 2007. [3] S.-H. Wu, A. R. Caparanga, R. B. Leron, and M.-H. LI, "Vapor pressures of aqueous blendedamine solutions containing (TEA/AMP/MDEA) + (DEA/MEA/PZ) at temperatures (313.15343.15) K," Experimental Thermal and Fluid Science, vol. 48, pp. 1-7, 2013. [4] Y.-H. Hsu, R. B. Leron, and M.-H. Li, "Solubility of carbon dioxide in aqueous mixtures of (reline + monoethanolamine) at T = (313.2 to 352.2) K," J. Chem. Thermodynamics, vol. 72, pp. 94-99, 2014. [5] J. G. M. S. Monteiro, H. Knuutila, N. J. M. C. P.-v. Elk, G. Versteeg, and H. F. Svendsen, " Kinetics of CO₂ absorption by aqueous N,N-diethylethanolamine solutions: Literature review, experimental results and modelling," Chem. Eng. Sci., vol. 127, pp. 1-12, 2015. [6] A. Hartono, E. F. da Silva, H. Grasdalen, and H. F. Svendsen, "Qualitative determination of species in DETA-H₂O-CO₂ system using ¹³C NMR spectra," Industrial & engineering chemistry research, vol. 46, no. 1, pp. 249–254, 2007.